

# TOPOGRAPHY OF THE THERMAL BOUNDARY LAYER AT THE BASE OF THE MANTLE

MARCO VIA GEOLOGY 393 THESIS I  
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## IMPORTANCE OF PROJECT

- To understand better the Earth's thermal evolution
- It will help to confirm or deny the theory of convection cells in the mantle

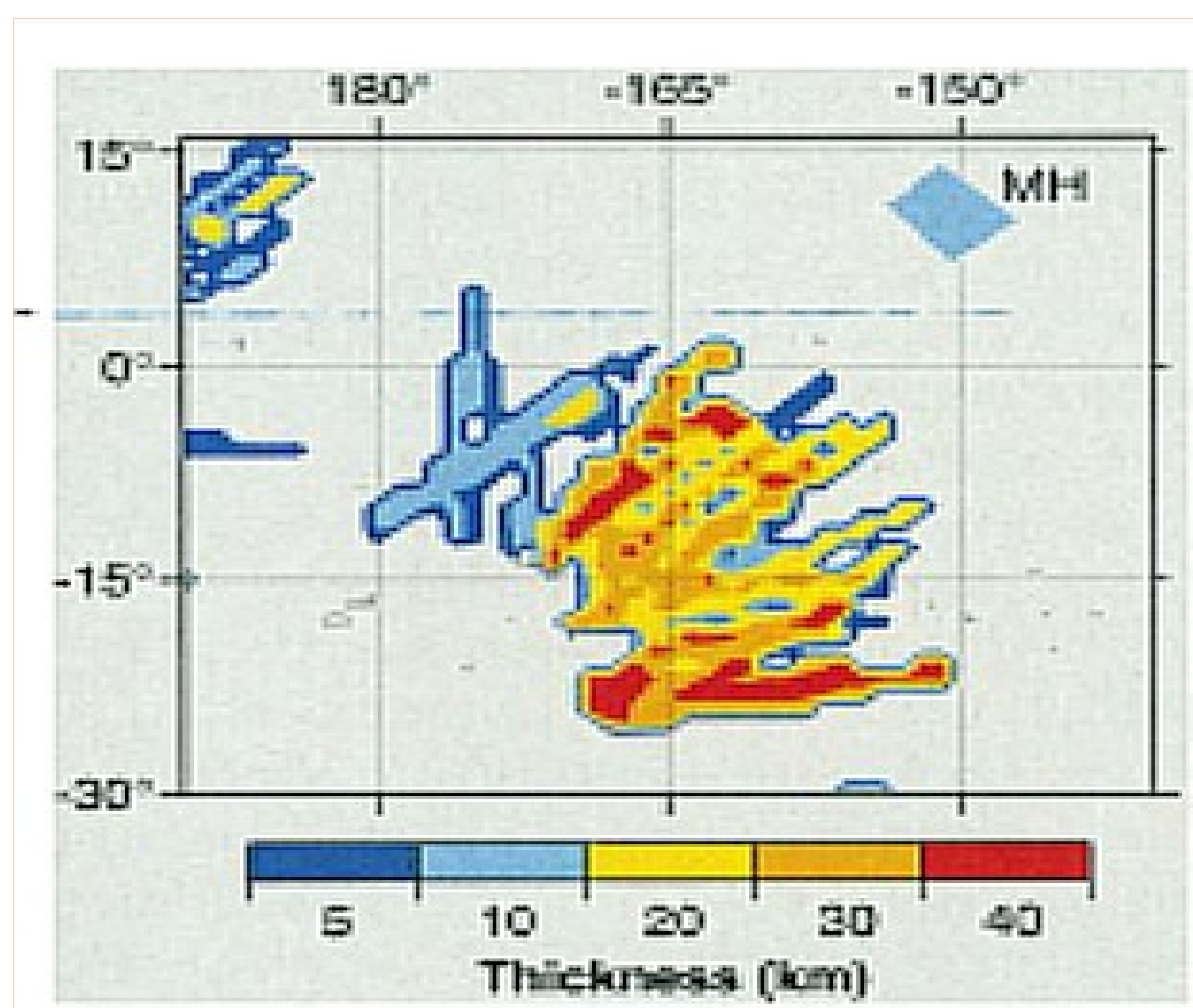
## TERMINOLOGY

- TBL: Thermal Boundary Layer
- ULVZ: Ultra low velocity zone
- CMBL: Core mantle boundary layer

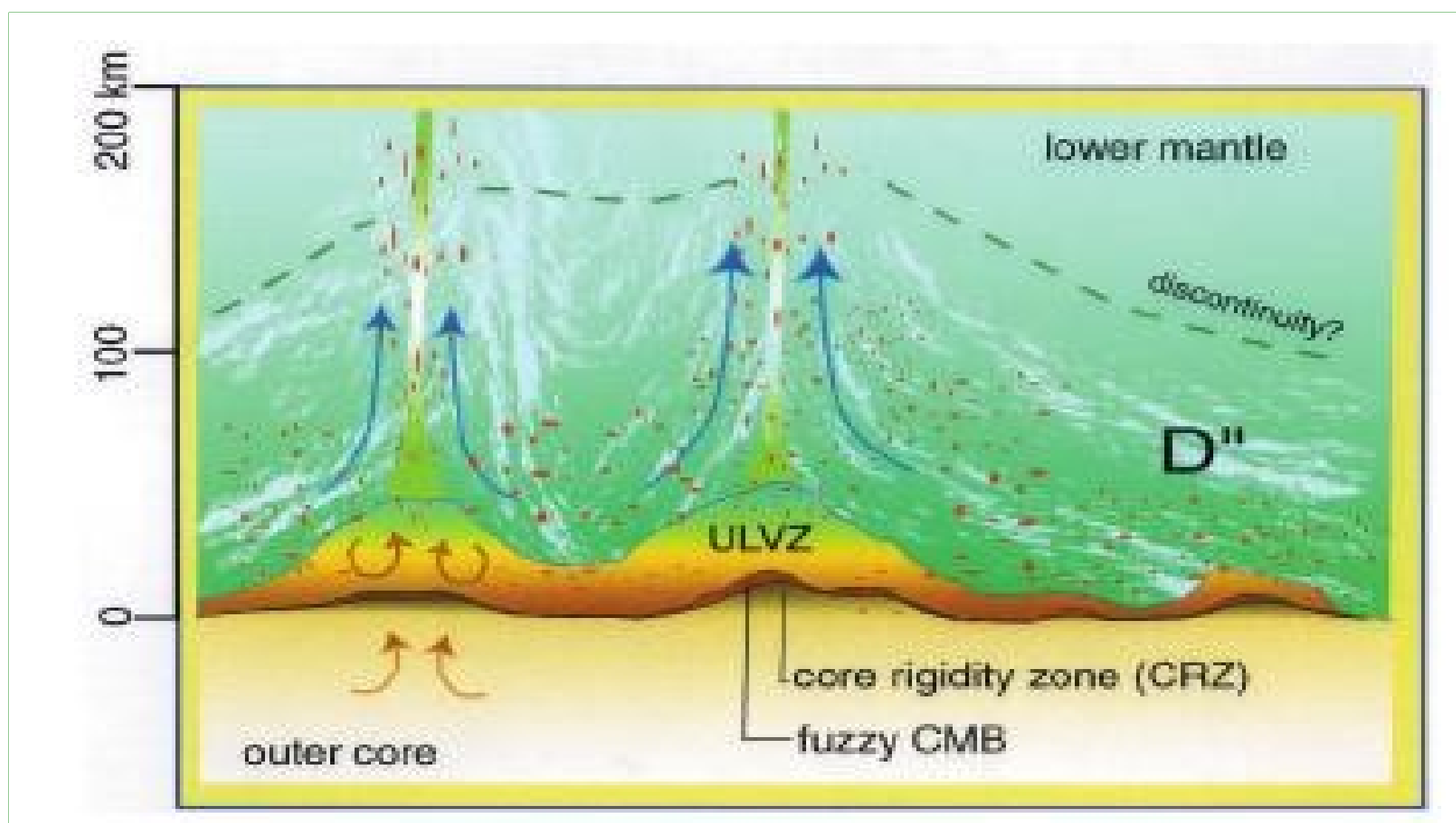
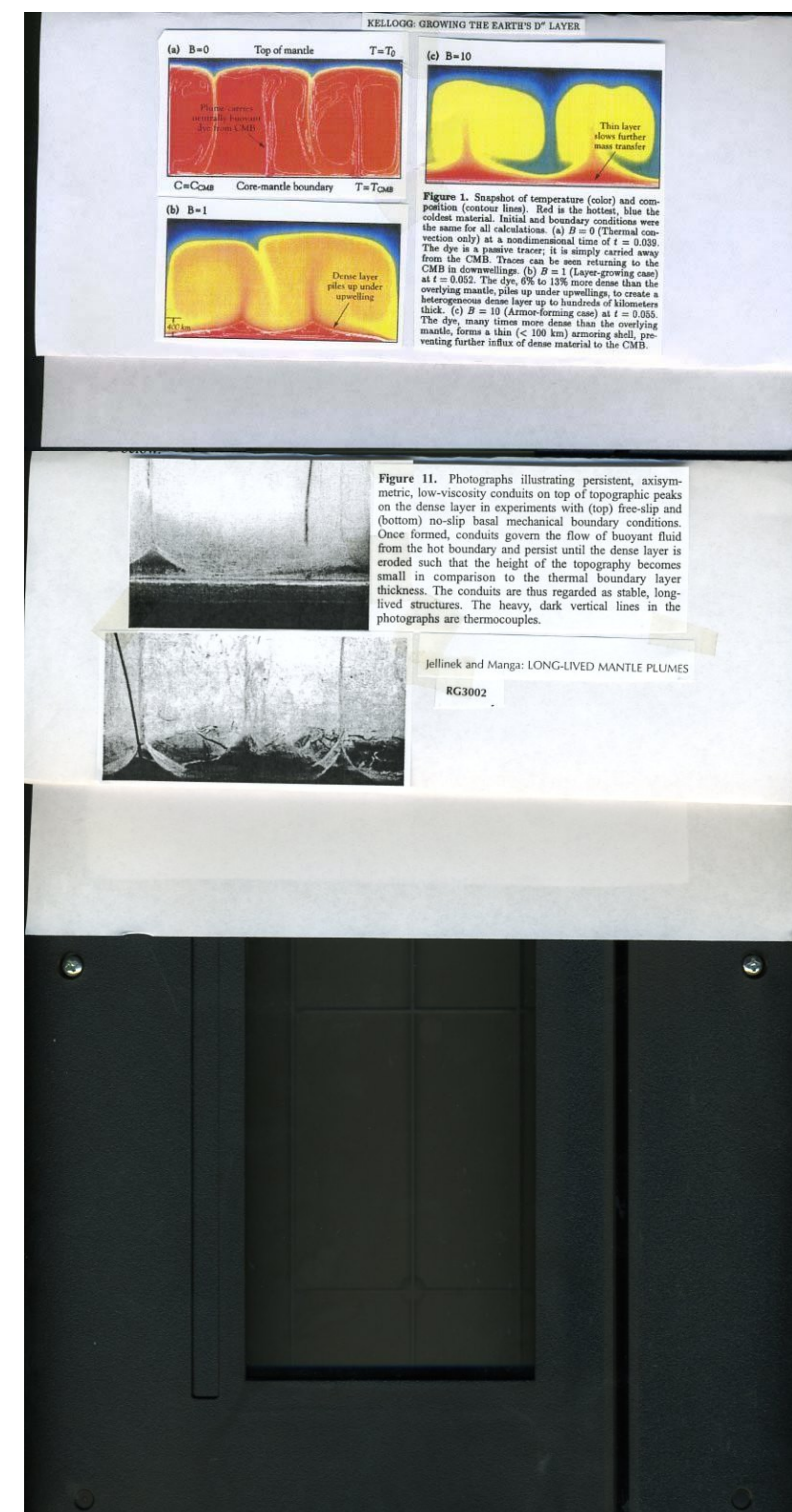
## BACKGROUND

- There is strong evidence through seismic data of the existence of a layer with an uneven topography known as D"
- This layer seems to have different composition than the lower mantle and/or outer core
- There is still some limitations as to whether D" covers the outer core in its entirety or just in some areas

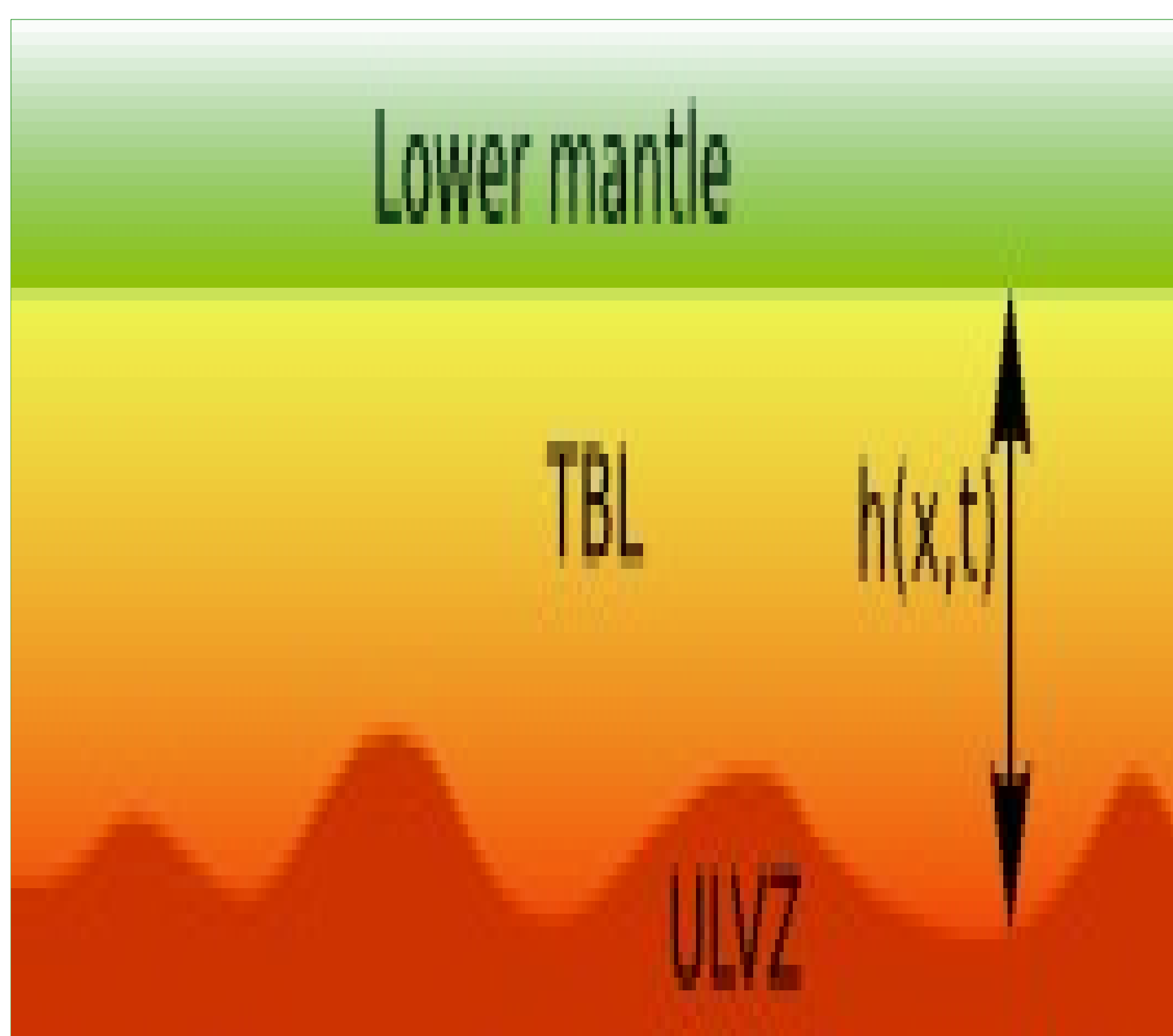
Red = reduction by 30% in the velocity or P- waves  
(Williams, et al 1996)



- Two-dimensional and three-dimensional numerical experiments have generated plumes
- The thermal convection systems used were under steady state conditions
- Two fluids with different viscosities were used



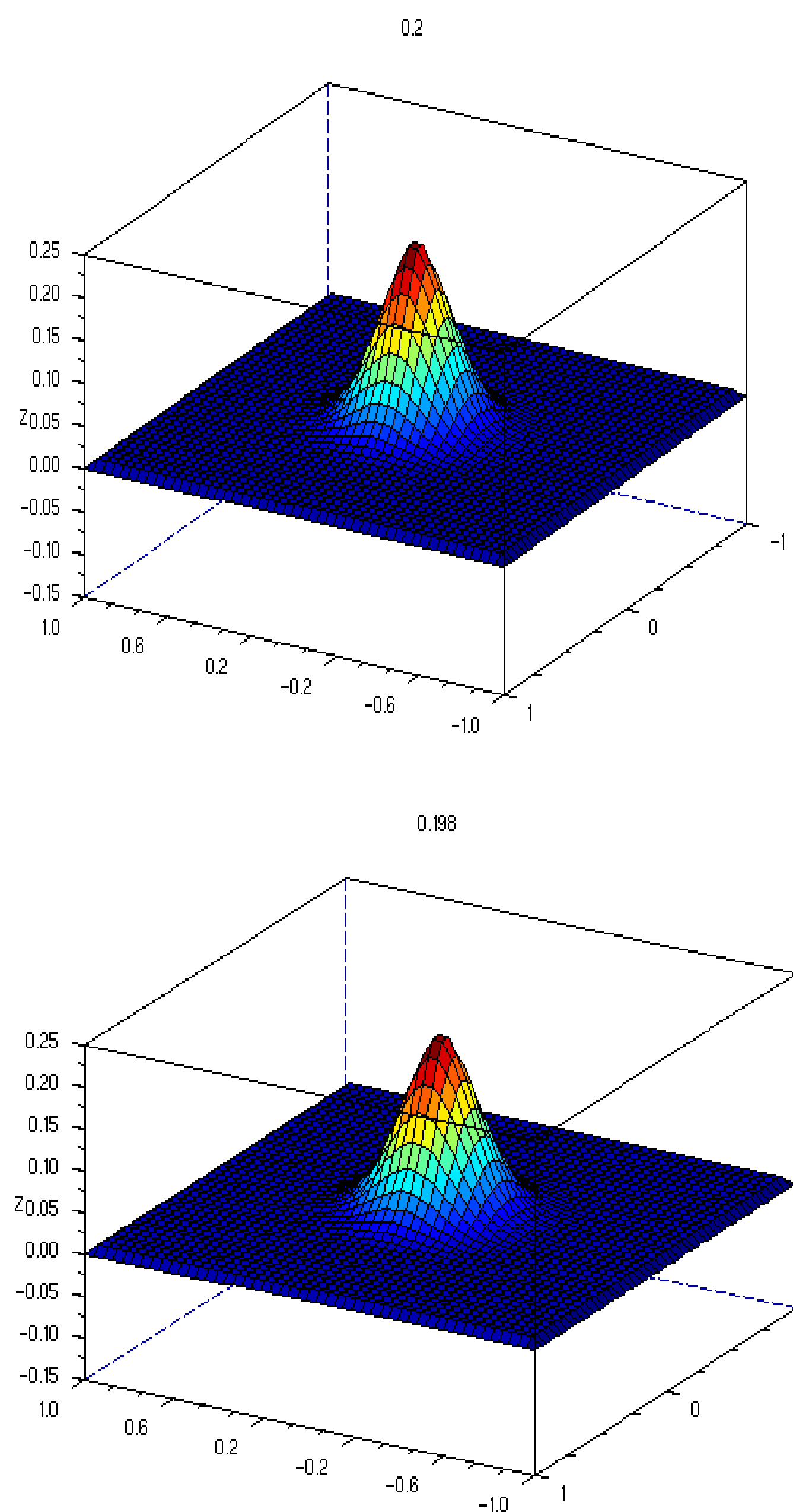
## Application of the Lubrication theory



Partial numerical results as iteration number is changed for different times, viscosities, and densities of the dense fluid layer.

## Stable topography

Changing the iteration number while keeping the other variables constant, the viscosity values changes and the formation of an stable topography occurs



## POSSIBLE RESULTS

- Once the ULVZ becomes stable the TBL fluid will start to form a plume
- The plume will be stable enough t

## HYPOTHESIS

- The core mantle boundary layer CMBL has an uneven topography
- Observations from numerical and experimental results show that it is necessary an uneven topography to form plumes.
- The stability of plumes seems to be close related to a definite topography

## ASSUMPTIONS

- Treat the thermal boundary layer as a thin fluid (TBL)
- Treat the ultra low velocity zone (ULVZ) as a denser fluid
- No interchange of materials between the outer core and the ULVZ

## CALCULATIONS

- Mass conservation  
$$[\partial \tilde{u} / \partial z^2 = (\rho g / \mu) \nabla_{\parallel} \cdot h] \quad (1)$$
Where:  $\partial \tilde{u} / \partial z^2$  = Shear stress (vector equation)/viscous resistance  
 $(\rho g / \mu) \nabla_{\parallel} \cdot h$  = gradient pressure on the system.  
 $\nabla_{\parallel}$  = is the horizontal gradient operator. Defined parallel to the walls of the narrow TBL  
$$\partial h / \partial t + \nabla_{\parallel} \cdot q = Q \delta(x - x_0) \quad (2)$$

Q is the mass flux into the plume conduit (vol/unit time)  
Equation (2) is the mass balance equation of the system  
Where q= the volume flux per unit channel area  
If:  $q = \int_0^h u \, dz$   $(3)$

The term on the right is a sink term of the fluid layer, indicating suction of material into the plume channel

Solving for equation (1) integrating twice, using the following boundary conditions;

$$\begin{aligned} \partial u / \partial z &= 0 \quad \text{and} \quad u = 0 \quad \text{at} \quad z = 0 \\ \partial h / \partial t + g \nabla_{\parallel} h^4 / (24 \nu) &= Q \delta(x - x_0) \quad (4) \end{aligned}$$

Combining equations (2) and (4) we obtain  
$$(\partial h / \partial t) + (g / 24 \nu) (\nabla_{\parallel} h^4) = Q \delta(x - x_0) \quad (5)$$

equation 5 is a PDE for h, which we need to solve with an initial condition and boundary conditions.

After solving the equations, the non-dimensionalization technique was applied to the results.

Begin to Demonstrate Feasibility with:

$$H = Lh^*$$

Where L is a constant and  $h^*$  is a non-dimensional variable

Also we have these known variables:

$$t = (L/u) t^*$$

$$\nabla_{\parallel} = (1/L^2) \nabla^*$$

$$\delta = (1/L^2) \delta^*$$

Dropping the asterisks:

$$\partial h / \partial t + (\rho g L^2 / 24 \mu V_0) \nabla_{\parallel} h^4 = (Q \delta / U \cdot L^2)$$

Defining  $L^2 = Q / U_0$

$$\text{then: } \partial h / \partial t + (\rho g Q \nabla_{\parallel} h^4) / 24 \mu V_0 = \delta \quad (6)$$

$$I = \rho g Q \nabla_{\parallel} h^4 \quad (\text{Intrusion term})$$

Discretizing this equation we have:

$$[k = -(\Delta t / d^2) I] \quad \text{where } I = \text{sigma term}$$

## REFERENCES

- Olson, P. 1990
- Jellinek and Manga 2004
- Garnero, E. 2000
- Kellogg, L. 1997

- Laboratory experiments have also produced plumes in a system with two fluids with different viscosities